

PCTWORLD INTELLECTUAL PROPERTY ORGANIZATION
International Bureau

INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification ⁶ : A61M 1/00		A2	(11) International Publication Number: WO 00/02603
			(43) International Publication Date: 20 January 2000 (20.01.00)
(21) International Application Number: PCT/US99/15426			(81) Designated States: AE, AL, AM, AT, AT (Utility model), AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, CZ (Utility model), DE, DE (Utility model), DK, DK (Utility model), EE, EE (Utility model), ES, FI, FI (Utility model), GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SK (Utility model), SL, TJ, TM, TR, TT, UA, UG, UZ, VN, YU, ZA, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SL, SZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).
(22) International Filing Date: 9 July 1999 (09.07.99)			
(30) Priority Data: 09/113,758 10 July 1998 (10.07.98) US			
(71) Applicant: BIOSCIENCE RESEARCH ASSOCIATES [US/US]; 6530 Clearhaven Circle, Dallas, TX 75248-4018 (US).			
(71)(72) Applicants and Inventors: MATSON, James, R. [US/US]; 6530 Clearhaven Circle, Dallas, TX 75248-4018 (US). LEE, Patrice, R. [US/US]; 91 Autumn Court, Erie, CO 80516 (US).			
(74) Agent: FELGER, Thomas, R.; Baker & Botts, L.L.P., 2001 Ross Avenue, Dallas, TX 75201-2980 (US).			Published <i>Without international search report and to be republished upon receipt of that report.</i>
(54) Title: HEMOFILTRATION SYSTEMS, METHODS, AND DEVICES USED TO TREAT INFLAMMATORY MEDIATOR RELATED DISEASE			
(57) Abstract			
<p>A hemofiltration system for a mammal comprises a hemofilter and an adsorbent device. The hemofilter removes ultrafiltrate from a blood stream extracted from the mammal to create a filtered blood stream and an ultrafiltrate stream. The adsorbent device is comprised of one or more adsorbent materials and is used to adsorb inflammatory mediators from the ultrafiltrate stream received from the hemofilter removing inflammatory mediators that cause inflammatory mediator related disease, sepsis, and SIRS/MODS/MOSF to create a post adsorption ultrafiltrate stream. The post adsorption ultrafiltrate stream is selectively combined with the filtered blood stream and together with the filtered blood stream is returned to the mammal. A hemofiltration process for a mammal is comprised of the following steps: (a) removing blood from the mammal to create a blood stream; (b) filtering the blood stream to remove ultrafiltrate from the blood to create an ultrafiltrate stream and a filtered blood stream; (c) adsorption of the inflammatory mediators from the ultrafiltrate stream that cause inflammatory mediator related disease, sepsis, SIRS/MODS/MOSF to create a post adsorption ultrafiltrate stream; (d) combining the post adsorption ultrafiltrate stream with the filtered blood stream to create a post adsorption ultrafiltrate/filtered blood stream; and (e) returning the post adsorption ultrafiltrate/filtered blood stream to the mammal.</p>			

FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AL	Albania	ES	Spain	LS	Lesotho	SI	Slovenia
AM	Armenia	FI	Finland	LT	Lithuania	SK	Slovakia
AT	Austria	FR	France	LU	Luxembourg	SN	Senegal
AU	Australia	GA	Gabon	LV	Latvia	SZ	Swaziland
AZ	Azerbaijan	GB	United Kingdom	MC	Monaco	TD	Chad
BA	Bosnia and Herzegovina	GE	Georgia	MD	Republic of Moldova	TG	Togo
BB	Barbados	GH	Ghana	MG	Madagascar	TJ	Tajikistan
BE	Belgium	GN	Guinea	MK	The former Yugoslav Republic of Macedonia	TM	Turkmenistan
BF	Burkina Faso	GR	Greece	ML	Mali	TR	Turkey
BG	Bulgaria	HU	Hungary	MN	Mongolia	TT	Trinidad and Tobago
BJ	Benin	IE	Ireland	MR	Mauritania	UA	Ukraine
BR	Brazil	IL	Israel	MW	Malawi	UG	Uganda
BY	Belarus	IS	Iceland	MX	Mexico	US	United States of America
CA	Canada	IT	Italy	NE	Niger	UZ	Uzbekistan
CF	Central African Republic	JP	Japan	NL	Netherlands	VN	Viet Nam
CG	Congo	KE	Kenya	NO	Norway	YU	Yugoslavia
CH	Switzerland	KG	Kyrgyzstan	NZ	New Zealand	ZW	Zimbabwe
CI	Côte d'Ivoire	KP	Democratic People's Republic of Korea	PL	Poland		
CM	Cameroon	KR	Republic of Korea	PT	Portugal		
CN	China	KZ	Kazakhstan	RO	Romania		
CU	Cuba	LC	Saint Lucia	RU	Russian Federation		
CZ	Czech Republic	LI	Liechtenstein	SD	Sudan		
DE	Germany	LK	Sri Lanka	SE	Sweden		
DK	Denmark	LR	Liberia	SG	Singapore		
EE	Estonia						

HEMOFILTRATION SYSTEMS, METHODS, AND DEVICES
USED TO TREAT INFLAMMATORY MEDIATOR RELATED DISEASE

TECHNICAL FIELD OF THE INVENTION

The present invention relates generally to systems, methods, and devices used for hemofiltration. More specifically, the present invention relates to novel systems, methods, and devices for hemofiltration for inflammatory mediator-related diseases (IMRD), which include systemic inflammatory response syndrome ("SIRS"), multiorgan system dysfunction syndrome ("MODS"), and multiorgan system failure ("MOSF") (collectively "SIRS/MODS/MOSF").

BACKGROUND OF THE INVENTION

Patients with life threatening illness are cared for in hospitals in the intensive care unit ("ICU"). These patients may be seriously injured from automobile accidents, etc., have had major surgery, have suffered a heart attack, or may be under treatment for serious infection, cancer, or other major disease. While medical care for these primary conditions is sophisticated and usually effective, a significant number of patients in the ICU will not die of their primary disease. Rather, a significant number of patients in the ICU die from a secondary complication known commonly as "sepsis" or "septic shock". Once again, the proper medical terms for sepsis and septic shock are systemic inflammatory response syndrome ("SIRS"), multiorgan system dysfunction syndrome

("MODS"), and multiorgan system failure ("MOSF") (collectively "SIRS/MODS/MOSF").

In short, medical illness, trauma, complication of surgery, and, for that matter, any human disease state, if sufficiently injurious to the patient, may elicit SIRS/MODS/MOSF. The systemic inflammatory response within certain physiologic limits is beneficial. As part of the immune system, the systemic inflammatory response promotes the removal of dead tissue, healing of injured tissue, detection and destruction of cancerous cells as they form, and mobilization of host defenses to resist or to combat infection. If the stimulus to the systemic inflammatory response is too potent, such as massive tissue injury or major microbial infection, however, then the systemic inflammatory response may cause symptoms which include fever, increased heart rate, and increased respiratory rate. This symptomatic response constitutes systemic inflammatory response syndrome ("SIRS"). If the inflammatory response is excessive, then injury or destruction to vital organ tissue may result in vital organ dysfunction, which is manifested in many ways, including a drop in blood pressure, deterioration in lung function, reduced kidney function, and other vital organ malfunction. This condition is known as multiorgan dysfunction syndrome ("MODS"). With very severe or life threatening injury or infection, the inflammatory response is extreme and can cause extensive tissue damage with vital organ damage and failure. These patients will usually die promptly without the use of ventilators to maintain lung ventilation, drugs to maintain blood pressure and strengthen the heart, and, in certain circumstances, artificial support for the liver, kidneys, coagulation, brain and other vital systems. This condition is known as multiorgan system failure syndrome ("MOSF"). These support measures partially compensate for damaged and failed organs, they do not cure

the injury or infection or control the extreme inflammatory response which causes vital organ failures.

5 In the United States of America each year, SIRS/MODS/MOSF afflicts approximately 400,000-600,000 patients and results in about 150,000 deaths. Overall, depending on the number of organ systems failing, the mortality rate of MOSF ranges generally from 40 to 100%. For instance, if three (3) or more vital organs fail, death results in more the 90% of cases. SIRS/MODS/ MOSF is the most common cause of death in intensive care units and is the thirteenth most common cause of death in the United States of America. SIRS/MODS/MOSF costs about \$5 to \$10 billion yearly for supportive care. In addition, the incidence of SIRS/MODS/MOSF is on the rise; reported cases increased about 139% between 1979 and 1987. This increase is due to an ageing population, increased utilization of invasive medical procedures, immuno-suppressive therapies (e.g. cancer chemotherapy) and transplantation procedures. (*Morbidity and Mortality Weekly Report* 1990; *Detailed Diagnoses and Procedures*, National Hospital Discharge Survey, 1993, from CDC/National Center for Health Statistics, 10/95.)

25 The detrimental mechanism of SIRS/MODS/MOSF is the excessive activation of the inflammatory response. The inflammatory response consists of the interaction of various cell systems (e.g., monocyte/macrophage, neutrophil, and lymphocytes) and various humoral systems (e.g., cytokine, coagulation, complement, and kallikrein/kinin). Each component of each system may function as an effector (e.g., killing pathogens, destroying tissue, etc.), a signal (e.g., most cytokines), or both. Humoral elements of the inflammatory response were known as toxic mediators, but are now known collectively as inflammatory mediators ("IM"). IM include various cytokines (e.g., tumor necrosis factor ("TNF"); the

interleukins; interferon, etc.), various prostaglandins (e.g., PG I₂, E₂, Leukotrienes), various clotting factors (e.g., platelet activating factor ("PAF")), various peptidases, reactive oxygen metabolites, and various poorly understood peptides which cause organ dysfunction (myocardial depressant factor ("MDF")). These compounds interact as a network with the characteristics of network preservation and self amplification. Some of these compounds, such as MDF and peptidases, are directly injurious to tissue; other compounds, such as cytokines, coordinate destructive inflammation. Infection (e.g., abscesses and sepsis) is a common complication of critical illness. Certain bacterial exotoxins, endotoxins or enterotoxins are extremely potent stimuli to SIRS/MODS/MOSF. Infection is the single most common cause of SIRS leading to MODS/MOSF. The development and use of effective antibiotics and other supportive measures have not had a significant effect on the death rate from MOSF.

The systemic inflammatory response with its network of systems (e.g., monocyte/ macrophage, complement, antibody production, coagulation, kallikrein, neutrophil activation, etc.) is initiated and regulated through the cytokine ("CK") system and IM's. The CK system consists of more than thirty known molecules each of which activates or suppresses one or more components of the immune system and one or more CK in the network. The CK network is the dominant control system of the immune response. The sources of CK's are monocyte/macrophages and endothelial cells and they are produced in every tissue in the body. Key characteristics of the CK system are as follows: (I) CK are chemical signals coordinating immune system and associated system activities; (ii) commonly, two or more CK will trigger the same action providing a "fail safe" response to a wide variety of different stimuli (the systemic inflammatory response is critical to the individuals

survival; these redundant control signals assure a system response which does not falter.); (iii) CK and IM concentrations (usually measured in blood) therefore increase in order to stimulate, control, and maintain the inflammatory response proportionally to the severity of the injury or infection; and (iv) as severity of injury or infection increases, the cytotoxic activity of the system increases resulting in MODS/MOSF. Therefore, high concentrations of CK and IM measured in the patient's blood, which are sustained over time, correlate with the patients risk of death.

Major research efforts by the biotechnology industry have sought cures for SIRS/MODS/MOSF, but none to date have been licensed by the United States Food and Drug Administration ("FDA") for use in humans. There is currently no definitive therapy for SIRS/MODS/MOSF (Dellinger, 1997; Natanson, 1994), even though a great deal of research funds have been spent on failed therapies for sepsis (Knaus, 1997). Critical care medicine techniques available to manage SIRS/MODS/MOSF are generally supportive in that they do not cure SIRS/MODS/MOSF. The biotechnology industry, however, has developed a number of prospective treatments for SIRS/MODS/MOSF. The general strategy of these prospective treatments is to identify what is conceived to be a key or pivotal single CK or IM. This single target CK or IM is then inactivated in an attempt to abate the inflammatory response. The most widely applied technologies used to inactivate CK or IM is binding with monoclonal antibodies ("MoAb") or specific antagonists ("SA"). MoAb's and SA's are used because they effectively bind the target CK or IM, or its receptor, usually in an "all or none" blockade. This strategy is problematic for two (2) reasons. First, the CK system is essential to mobilize the inflammatory response, and through it, the host immune response. If the CK system were blocked, death

would ensue from unhealed injury or infection. Second, the CK and IM signals which make up the control network of the immune response consist of many redundant control loops to assure the "fail safe" initiation and continuation of this critical response. In the field of engineering, control theory indicates that a redundant, self amplifying system will not be effectively controlled by blocking one point, such as one CK or IM (Mohler, 1995).

Also, of interest, note the existing technique of hemofiltration ("HF"), which was developed as a technique to control over hydration and acute renal failure in unstable ICU patients. Existing HF techniques may use a hemofilter of some sort, which consists of a cellulose derivatives or synthetic membrane (e.g., polysulfone, polyamide, etc.) fabricated as either a parallel plate or hollow fiber filtering surface. Since the blood path to, through, and from the membrane is low resistance, the patients' own blood pressure drives blood through the filter circuit. In these HF applications, the hemofilter is part of a blood circuit. In passive flow HF, arterial blood flows through a large bore cannula, into plastic tubing leading to the filter; blood returns from the filter through plastic tubing to a vein. This is known as arteriovenous HF. Alternately, a blood pump is used, so that blood is pumped from either an artery or a vein to the filter and returned to a vein. This is known as pumped arterio-venous HF or pumped veno-venous HF. Ultrafiltrate collects in the filter jacket and is drained through the ultrafiltrate line and discarded. Ultrafiltrate flow rates are usually 250 ml - 2000 ml/hour. In order to prevent lethal volume depletion, a physiologic and isotonic replacement fluid is infused into the patient concurrently with HF at a flow rate equal to or less than the ultrafiltrate flow rate. The balance of replacement fluid

and ultrafiltrate is determined by the fluid status of the patient.

5 The pores of most filter membranes allow passage of molecules up to 30,000 Daltons with very few membranes allowing passage of molecules up to 50,000 Daltons. The membranes used to treat renal failure were generally designed to achieve the following specific goals: (I) to permit high conductance of the aqueous phase of blood plasma water needed to permit the formation of
10 ultrafiltrate at a fairly low transmembrane pressure (typically 20-40 mm Hg), which requires a relatively large pore size that incidentally passes molecules of up to 30,000 to 50,000 Daltons; and (ii) to avoid passage of albumin (e.g., 68,000 Daltons). Note with these existing
15 hemofilters used to treat renal failure, the ultrafiltrate contains electrolytes and small molecules (e.g., urea, creatinine, and uric acid), but no cells and only peptides and proteins smaller than the membrane pore size. The composition of the ultrafiltrate is very similar to plasma
20 water. Loss of albumin, and subsequently, oncotic pressure, could cause or aggravate tissue edema and organ dysfunction (e.g., pulmonary edema), so hemofilters are designed to avoid this by having molecular weight exclusion limits well below the molecular weight of albumin (e.g.,
25 68,000 Daltons).

 During filtration of protein containing solutions, colloids or suspensions, or blood, the accumulation of protein as a gel or polarization layer occurs on the membrane surface. This gel layer typically reduces
30 effective pore size, reducing the filterable molecular weights by roughly 10-40%. Therefore, pore sizes selected are somewhat larger than needed, anticipating a reduction in effective size. Thus, present membranes allow filtration and removal of excess water, electrolytes, small molecules
35 and nitrogenous waste while avoiding any loss of albumin or

larger proteins. These membranes are well-suited to their accepted uses, that is, treatment of over hydration and acute renal failure in unstable ICU patients.

Uncontrolled observations in ICU patients indicate
5 that HF, in addition to controlling over hydration and acute renal failure, is associated with improvements in lung function and cardiovascular function. None of these improvements has been associated with shortened course of ventilator therapy, shortened ICU stay, or improved
10 survival. The usual amount of ultrafiltrate taken in the treatment of over hydration and acute renal failure is 250 to 2000 ml/hour, 24 hours a day. A few published observations have suggested that higher amounts of ultrafiltrate brought about greater improvements in
15 pulmonary and cardiovascular status; these have resulted in the development of a technique known as high volume HF ("HVHF"). In HVHF, from 2 to 9 liters/hour of ultrafiltrate are taken for periods of from 4 to 24 hours or more. Furthermore, preliminary uncontrolled or poorly controlled
20 studies suggest that HVHF improves survival in patients with SIRS/MODS/MOSF; there is growing interest in the use of HVHF in SIRS/MODS/MOSF. There is however great hesitance to use HVHF for the following reasons: (I) the high volumes (currently 24 - 144 liters/day) of ultrafiltrate require
25 equally high volumes of sterile, pharmaceutical grade replacement fluid; at these high volumes, errors in measuring ultrafiltrate coming out and replacement fluid flowing into the patient could cause injurious or lethal fluid overload or volume depletion; (ii) the high volume
30 of ultrafiltrate removed could filter out of the blood desirable compounds from the patient resulting in dangerous deficiencies; this is currently theoretical, but should be taken seriously; (iii) large volumes of warm (body temperature) ultrafiltrate flowing out of the patient, and
35 large volumes of cool (room temperature) replacement fluid

flowing into the patient can cause thermal stress or hypothermia; and (iv) high volumes of replacement fluid add considerable expense to the therapy.

5 HVHF, as currently practiced, uses conventional hemofilters with pore sizes which provide a molecular weight cut of 30,000 Daltons and occasionally of 50,000 Daltons. The device and process described in United States Patent Number 5,571,418 generally contemplates the use of large pore hemofiltration membranes with pore sizes to provide molecular weight exclusion limits of 100,000 to 10 150,000 Daltons. With these higher molecular weight cutoffs, these membranes are designed to remove a wider range of different IM's; these large pore membranes should remove excess amounts of all known IM's. These large pore hemofiltration membranes have been demonstrated in animal 15 studies to be superior to conventional hemofilter membranes in improving survival time in a swine model of lethal *Staphylococcus aureus* infection (Lee, PA et al. *Critical Care Medicine* April 1998). It is anticipated that they will be superior to conventional membranes in 20 SIRS/MODS/MOSF. However, it may be anticipated that in HVHF, the large pore membranes may also remove more different desirable compounds thus increasing the risk of the negative side effects of HVHF.

25 Other techniques used in the past to treat acute renal failure and/or SIRS/MODS/MOSF include hemodialysis and plasmapheresis. Hemodialysis is well suited to fluid and small solute (less the 10,000 Daltons) removal. However hemodialysis membranes remove very few IM (only those 30 smaller the 5000 to 10,000 Daltons) and so have been ineffective in improving patient condition in SIRS/MODS/MOSF. In the unstable ICU patient, hemodialysis commonly results in rapid deterioration of cardiovascular function and pulmonary function requiring premature 35 termination of the dialysis procedure. Hemodialysis has

also been associated with increasing the occurrence of chronic renal failure in survivors of SIRS/MODS/MOSF. HF was specifically developed (Kramer, 1997) to avoid these complications of hemodialysis and has been very successful in doing so.

Plasmapheresis can be done with both membrane based and centrifugation based techniques. Plasmapheresis separates plasma and all that plasma contains from blood, leaving only formed elements. The removed plasma is usually replaced by either albumin solution or fresh frozen plasma. The removed plasma would contain all IM's. Studies of plasmapheresis in animal models of SIRS/MODS/MOSF have shown increased mortality with plasmapheresis compared to untreated control animals. No controlled study of plasmapheresis in humans with SIRS/MODS/MOSF has ever been done. The expense of albumin and fresh frozen plasma, and the risk of transmission of serious or deadly viral disease with fresh frozen plasma are serious draw backs to the use of plasmapheresis in SIRS/MODS/MOSF.

Consequently, the prior art remains deficient in the lack of effective methods of treating IM related disease (e.g., SIRS/MODS/MOSF), which is safe. Furthermore, while high volume hemofiltration holds some promises, it is unworkable in its present form and is overly dangerous. The present invention fulfills this longstanding need and desire in this art.

SUMMARY OF THE INVENTION

Preferred embodiments of the process and system treat inflammatory mediator-related disease, such as sepsis or SIRS/MODS/MOSF.

Specifically, preferred embodiments of the hemofiltration system are used in mammals. Preferred embodiments are generally comprised of a hemofilter, blood and ultrafiltrate lines, and an adsorptive device of one or

more chambers containing adsorbent material of one or more types. The hemofilter receives a stream of blood removed from the mammal and removes ultrafiltrate from the stream of blood from the mammal and thereby creates a stream of
5 filtered blood, which is eventually returned to the mammal, and a stream of ultrafiltrate. The hemofilter sieves the ultrafiltrate, the ultrafiltrate comprised of a fraction of plasma water, electrolytes, and peptides and small proteins. The sieved blood peptides and proteins have a
10 molecular size smaller than the pore size of the membrane; IM are included in this group. The hemofilter is comprised of a biocompatible material. In particular, the hemofilter is comprised of a membrane and a jacket, wherein the membrane is selected from the group of biocompatible
15 materials (e.g., polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-alcohol, polyamide, polycarbonate, etc.) and cellulose derivatives, and the jacket is comprised of polycarbonate or some other suitable biocompatible material.

20 The adsorptive device is comprised of an encasement jacket. The adsorptive device incorporates one or more chambers containing adsorbent material of one or more types in the chamber or chambers. The adsorptive device receives the stream of ultrafiltrate and selectively or
25 nonselectively removes IM that cause inflammatory mediator-related disease, such as sepsis and SIRS/MODS/MOSF, from the ultrafiltrate removed from the blood of the mammal to create a stream of post adsorption ultrafiltrate. The adsorptive device is preferably comprised of an encasement
30 jacket comprised of polycarbonate or other suitable biocompatible material and may be configured as having one or more chambers. Each chamber may contain an adsorbent material or a combination of adsorbent materials. The adsorptive device is designed to be placed in the line
35 transferring ultrafiltrate removed by the hemofilter and

adsorbs IM from the ultrafiltrate producing " post adsorption ultrafiltrate." The stream of post adsorption ultrafiltrate is eventually combined or reinfused, in whole or in part, with the stream of filtered blood and returned to the mammal. The adsorbent material may be comprised of a host of materials, including, but not limited to, activated charcoal, uncharged resins, charged resins, silica, immobilized polymyxin B, anion exchange resin, cation exchange resin, neutral exchange resin, polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-alcohol, polyamide, polycarbonate, cellulose derivatives, immobilized monoclonal antibodies, immobilized IM receptors, and immobilized specific antagonists. The adsorbent material may also be organized in a number of ways, including a matrix of rods, a porous sieve, a matrix of porous material which conveniently presents adsorbent materials to ultrafiltrate, and beads. Each adsorbent material may be uncoated or coated; the adsorbent material and/or the adsorbent device should prevent or contain dissolution and fragmentation of adsorbent material.

In addition, preferred embodiments may also be comprised of a blood pump to pump the blood from the mammal, an ultrafiltrate waste pump to pump a portion of the ultrafiltrate to the waste reservoir, an ultrafiltrate return pump to pump ultrafiltrate back into the blood circuit returning the ultrafiltrate to the patient, a three-way stop cock or a first three-way joint, and a second three-way joint. First tubing transfers the blood from the mammal to the blood pump; second tubing transfers the blood from the blood pump to hemofilter; third tubing transfers the filtered blood filtered by the hemofilter to the three-way joint or three-way stop cock; fourth tubing transfers the filtered blood along with the post adsorption ultrafiltrate to the mammal; fifth tubing transfers the ultrafiltrate to the adsorptive device; sixth tubing

transfers the post adsorption ultrafiltrate to second three-way joint; seventh tubing transfers post adsorption ultrafiltrate to the first ultrafiltrate return pump; eighth tubing transfers post adsorption ultrafiltrate from the first ultrafiltrate return pump to three-way joint or three-way stop cock joining fourth tubing which transfers filtered blood along with the post adsorption ultrafiltrate to the mammal; ninth tubing transfers post adsorption ultrafiltrate to second ultrafiltrate waste pump; and tenth tubing transfers post adsorption ultrafiltrate from second ultra filtrate waste pump to waste reservoir. Note that there are alternate embodiments.

Finally, alternative preferred embodiments may utilize a single filter, which would be a "two-stage" filter, that incorporates both the hemofilter and the adsorptive device containing the adsorbent material(s). Note for the purpose of discarding a portion of ultrafiltrate, a second ultrafiltrate pump can be used along with associated changes to the necessary tubing.

Preferred processes to treat IM related diseases and SIRS/MODS/MOSF in a mammal are comprised of the following steps: (a) removing blood from the mammal to create a blood stream; (b) filtering the blood stream to remove ultrafiltrate from the blood to create an ultrafiltrate stream and a filtered blood stream; © circulating the ultrafiltrate stream to the adsorptive device to remove IM that cause IM related disease and SIRS/MODS/MOSF to create a post adsorption ultrafiltrate stream; (d) combining the post adsorption ultrafiltrate stream with the filtered blood stream to create a post adsorption ultrafiltrate/filtered blood stream; and (e) returning the post adsorption ultrafiltrate/ filtered blood stream to the mammal. Additional steps may include after step (a), (a1) pumping the blood stream; and after step (b), (b1)

circulating ultrafiltrate to the ultrafiltrate waste pump and on to the waste reservoir and after step (c), (c1) pumping the post adsorption ultrafiltrate stream circulating the post adsorption ultrafiltrate stream to the post hemofilter blood line, or alternatively, to any convenient tubing or vascular canula which returns post adsorption ultrafiltrate stream to the mammal's vascular system.

Preferred embodiments provide a number of advantages, important functions and key features. In particular, the use of preferred embodiments allows the safe use of two stage high volume hemofiltration ("HVHF") with its improved patient survival, avoids dangerous fluid balance errors inherent to conventional HVHF, avoids the risk of depletion of desirable humoral compounds, avoids or minimizes thermal stress and hypothermia, and avoids the cost of excessive amounts of replacement fluid. The immune system has many, redundant CK and IM control loops; several of these loops must be down regulated if system wide control is to be achieved and death from SIRS/MODS/MOSF prevented. The preferred embodiments address this task.

Moreover, the use of the adsorptive device comprised of adsorbent material(s) provides additional advantages. Conventional hemofiltration (i.e., hemofiltration performed to treat acute renal failure) usually requires the production of and discard of from about 200 ml to 2,000 ml of ultra filtrate per hour. In patients, if this volume were not replaced, the loss of fluid would soon lead to dehydration, shock and death. In practice, some or all of this hourly loss is replaced each hour as either medicinal or nutrient solutions, or, in whole or in part, with an isotonic, physiologic, sterile, pharmaceutical grade intravenous solution known as replacement fluid. The pumps used to control ultrafiltrate and replacement fluid flow are either intravenous fluid pumps or roller pumps adapted

for this purpose. These pumps can have an error of from 5-10% and still be considered acceptable for clinical purposes. Bedside nurses monitor actual fluid balance and correct errors. For conventional hemofiltration, these devices and techniques do not usually introduce serious errors, partly due to the level of fluid extracted, filtered, and replaced. However, various investigators have adapted hemofiltration for use in SIRS/MODS/MOSF by markedly increasing the volume of ultrafiltrate taken each hour. As discussed above, this technique is known as HVHF and requires that from 2 to 9 liters/hour of ultrafiltrate be taken from the patient. Small, uncontrolled studies with HVHF suggest that HVHF can significantly improve vital organ function, shorten the duration of vital organ failure, and improve patient survival in SIRS/MODS/MOSF.

Criticisms of HVHF include: (i) the risk of fluid balance errors with high fluid flux; (ii) the risk of depletion of desirable compounds; (iii) the risk of hypothermia; and (iv) expense. First, with respect to the risk of high fluid flux, the high volumes of ultrafiltrate (about 48 to 150 liters/day) and replacement fluid (about 48 to 150 liters/day), being pumped on current equipment, could result in large and dangerous fluid imbalances. With current equipment, imbalances of as much as 30 liters of excess fluid delivered to the patient, or 30 liters of excess fluid removed from the patient could occur. Any error approaching this magnitude in either direction would be very injurious or lethal to the patient. Hence, HVHF is considered by many to be dangerous and potentially deadly. Second, with respect to the risk of depletion of desirable compounds, the high volumes of ultrafiltrate (about 48 to 150 liters/day) removed from the patient do remove large amounts of IM with resulting improvements in SIRS/MODS/MOSF. However, these high volumes may also remove desirable compounds with deleterious effects. This

criticism is theoretical at this time but should be taken seriously. Third, with respect to the risk of hypothermia, about 48 to 150 liters of warm (body temperature) ultrafiltrate are removed from the patient causing heat loss, and about 48 to 150 liters of cool (room temperature) replacement fluid is infused into the patient causing cooling. This flux causes thermal stress and may cause hypothermia. Thermal stress creates additional energy demands on these already critically stressed patients and may compromise their condition. Fourth, with respect to the expense, the high volumes of ultrafiltrate (about 48 to 150 liters/day) require equal or nearly equal volumes of isotonic, physiologic, sterile, pyrogen free, pharmaceutical grade replacement fluid (RF). Such fluid is expensive and in these large quantities would add substantially to the cost of patient care.

As stated above, the use of the adsorbent device by preferred embodiments addresses these concerns. First, with respect to the risk of high fluid flux, the adsorbent device adsorbs IM from the ultrafiltrate thus removing them from the ultrafiltrate; the post adsorption ultrafiltrate may then be reinfused, in whole or in part, back into the patient. Since post adsorption ultrafiltrate is returned to the patient, in whole or in part, the amount of replacement fluid needed to preserve fluid balance in the patient is sharply reduced (to the amount of ultrafiltrate discarded), or eliminated entirely. The volumes of ultrafiltrate discarded and replacement fluid infused will need to be only those indicated by the patient's state of edema (over hydration) and/or needs to accommodate medicinal or nutrient solutions; typically 2 to 6 liters per day. These lower volumes of fluid flux (about 2 to 6 liters per day) can be safely managed by existing pump technology, pumping errors on these small volumes are well tolerated. Second, with respect to the risk of depletion

of desirable compounds, as all or most of the ultrafiltrate will be returned to the patient (as post adsorption ultrafiltrate), and as adsorbent material will be selected with as narrow a range of adsorbed substances as possible and focused on IM, the loss of desirable substances is minimized. Third, with respect to the risk of hypothermia, as warm (body temperature) ultrafiltrate is returned to the patient, the amount of cool (room temperature) replacement fluid needed will be sharply reduced. This will eliminate the heat loss which would otherwise occur with discard of ultrafiltrate and also eliminate the cooling which would occur by the infusion of cool replacement fluid. In this way, the stress of hypothermia is eliminated. Fourth, with respect to the expense, the cost of RF varies widely depending on markets, contract arrangements and other considerations. However, \$2 to \$10 per liter are typical costs. Thus, HVHF could create an incremental cost of from \$96 to \$1,500 per day. By reinfusion of post adsorption ultrafiltrate following adsorption of IM's, and so eliminating the need for all or most replacement fluid, this incremental cost is eliminated. In summary, HVHF is a technique which may significantly improve survival in SIRS/MODS/MOSF, however, HVHF creates new and substantial risks and expenses. Preferred embodiments eliminate or sharply reduce these risks and expenses, and make HVHF much safer and more cost effective in patients suffering from SIRS/MODS/MOSF.

Other advantages of the invention and/or inventions described herein will be explained in greater detail below.

BRIEF DESCRIPTION OF THE DRAWINGS

The accompanying drawings are incorporated into and form a part of the specification to illustrate several examples of the present inventions. These drawings together with the description serve to explain the

principles of the inventions. The drawings are only for the purpose of illustrating preferred and alternative examples of how the inventions can be made and used and are not to be construed as limiting the inventions to only the illustrated and described examples. Further features and advantages will become apparent from the following and more particular description of the various embodiments of the invention, as illustrated in the accompanying drawings, wherein:

FIGURE 1A is a schematic of the physical layout of various components of a preferred embodiment, including mammal 100, hemofilter 102, blood pump 104, first ultra-filtrate pump 106a and second ultrafiltrate pump 106b, adsorptive device 108 having one or more chambers containing adsorbent material of one or more types, three-way stop cock or first three-way joint 110, second three-way joint 125, and associated tubing;

FIGURE 1B is a schematic of the physical layout of various components of a preferred embodiment, including mammal 100, hemofilter 102, blood pump 104, single ultra-filtrate pump 106, adsorptive device 108 having one or more chambers containing adsorbent material of one or more types, three-way stop cock or first three-way joint 110, second three-way joint 125, and associated tubing;

FIGURE 2 is a schematic of an alternate physical layout of various components of a preferred embodiment, including mammal 200, hemofilter 202, blood pump 204, first ultra-filtrate pump 206a and second ultra-filtrate pump 206b, adsorptive device 208 having one or more chambers containing adsorbent material of one or more types, three-way stop cock or first three-way joint 210, second three-way joint 225, and associated tubing;

FIGURE 3A is a diagram showing the system flow of a preferred embodiment shown in FIGURE 1A;

FIGURE 3B is a diagram showing the system flow of a preferred embodiment shown in FIGURE 1B;

FIGURE 4 is a diagram showing the system flow of a preferred embodiment shown in FIGURE 2; and

5 FIGURES 5A, 5B, and 5C are diagrams showing alternate preferred embodiments of adsorbent device 108 (in FIGURES 1A and 1B) and adsorptive device 208 (in FIGURE 2).

DETAILED DESCRIPTION OF THE INVENTION

The preferred embodiment will be described by referring to apparatus showing various examples of how the inventions can be made and used. When possible, like reference characters are used throughout the several views of the drawing to indicate like or corresponding parts.

Related Definitions

As a point of reference, please note the following terms and definitions.

The term "hemofiltration" refers to a process of filtering blood by a membrane with separation of all formed elements, all proteins larger than effective pore size of the membrane, and retained plasma water and solute (these return to the patient) from ultrafiltrate.

The term "ultrafiltrate" refers to the filtered plasma water and solute and molecules (including target peptides and proteins containing IM) smaller than effective pore size of the membrane. The term "Systemic Inflammatory Response Syndrome" ("SIRS") refers to the excessive and dysfunctional elaboration by a human patient of inflammatory mediators ("IM") which results in an excessive and injurious inflammatory response.

The term "Multiple Organ Dysfunction Syndrome" ("MODS") refers to SIRS causing injury or destruction to vital organ tissue and resulting in vital organ dysfunction, which is manifested in many ways, including a drop in blood pressure, deterioration in lung function, reduced kidney function, and other vital organ malfunction.

The term "Multiple Organ System Failure" ("MOSF") refers to the clinical syndrome of vital organ dysfunction or failure due to tissue injury resulting from SIRS. Its mortality rate is approximately 40-100%.

The term "Inflammatory Mediator Related Disease" ("IMRD") refers to any disease state characterized by

injurious or lethal excess production of IM. Diseases commonly included in this category include Lupus Erythematosus, Hemolytic Uremic Syndrome, Bullous Pemphigoid, pemphigus vulgaris, sepsis, SIRS/MODS/MOSF, and the like.

The term "Inflammatory Mediators" or "IM" refers to a heterogeneous group of chemicals synthesized and released by human tissue. IM include cytokines, prostaglandins, oxygen metabolites, kinins, complement factors, various clotting factors, various peptidases, various peptides, various proteins, and various toxic peptides. The molecular weight range of known IM is 1,000-100,000 Daltons.

The term "Hemofilter" refers to the filter used in hemofiltration. It can be configured in a number of ways, such as a series of parallel plates or as a bundle of hollow fibers. The blood path is from a blood inlet port, through the fibers or between the plates, then to a blood outlet port. Filtration of blood occurs at the membrane with ultrafiltrate forming on the side of the membrane opposite the blood. This ultrafiltrate accumulates inside the body of the filter contained and embodied by the filter jacket. This jacket has an ultrafiltrate drainage port.

FIGURE 1A is a schematic of the physical layout of various components of a preferred embodiment, including mammal 100, hemofilter 102, blood pump 104, first ultrafiltrate pump 106a, second ultrafiltrate pump 106b, adsorptive device 108 having one or more chambers containing adsorbent material of one or more types, three-way stop cock or first three-way joint 110, second three-way joint 125, and associated tubing. FIGURE 1B is similar to FIGURE 1A, except that single ultrafiltrate pump 106 is used in lieu of first ultrafiltrate pump 106a and second ultrafiltrate pump 106b. Both FIGURES 1A and 1B position three-way stop cock or first three-way joint 110 in such a manner that it divides ultrafiltrate stream downstream from

adsorptive device 108. FIGURE 2 is an alternate schematic of the physical layout of various components of a preferred embodiment shown in FIGURES 1A and 1B, except that three-way stop cock or first three-way joint 210 divides ultrafiltrate stream before adsorptive device 208. FIGURES 3A and 3B are diagrams showing the system flow of a preferred embodiment shown in FIGURES 1A and 1B, respectively. FIGURE 4 is a diagram showing the system flow of a preferred embodiment shown in FIGURE 2.

Steps 301 and 302 (in FIGURES 3A and 3B) and steps 401 and 402 (in FIGURE 4) show blood being continuously withdrawn from mammal 100 (in FIGURES 1A and 1B) and mammal 200 (in FIGURE 2) and directed to blood pump 104 (in FIGURES 1A and 1B) and blood pump 204 (in FIGURE 2) via first tubing 101 (in FIGURES 1A and 1B) and first tubing 201 (in FIGURE 2). Specifically, step 303 (in FIGURE 3A and 3B) and step 403 (in FIGURE 4) show the continuous pumping of blood by blood pump 104 into hemofilter 102 via second tubing 103 (in FIGURES 1A and 1B) and by blood pump 204 into hemofilter 202 via second tubing 203 (in FIGURE 2). Mammal 100 (in FIGURES 1A and 1B) and mammal 200 (in FIGURE 2), such as a human being, preferably have a major blood vessel cannulated allowing for the continuous withdrawal of blood by blood pump 104 (in FIGURES 1A and 1B) and blood pump 204 (in FIGURE 2). As shown in steps 304 and 306 (in FIGURES 3A and 3B) and steps 404 and 406 (in FIGURE 4), hemofilter 102 ultra-filtrates blood extracted from mammal 100 (in FIGURES 1A and 1B) and hemofilter 202 ultra-filtrates blood extracted from mammal 200 (in FIGURE 2). And, step 305 (in FIGURES 3A and 3B) and step 405 (in FIGURE 4) returns blood filtered by hemofilter 102 to mammal 100 via third tubing 105 and fourth tubing 107 in FIGURES 1A and 1B and by hemofilter 202 to mammal 200 via third tubing 205 and fourth tubing 207 in FIGURE 2.

Referring to FIGURES 1A, 1B, and 2, ultrafiltration is a filtration process in which blood cells and blood proteins with a molecular size larger than the pore size of hemofilter membrane 109 (in FIGURES 1A and 1B) and hemofilter membrane 209 (in FIGURE 2) are retained in the blood path. The composition of hemofilter membrane 109 (in FIGURES 1A and 1B) and hemofilter membrane 209 (in FIGURE 2) are preferably comprised of biocompatible material, such as polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-alcohol, polyamide, polycarbonate, cellulose derivatives, etc., but is not limited to these materials. The jacket of the hemofilter will be preferably comprised of a biocompatible material, such as polycarbonate, but not limited to, polycarbonate. Hemofilter membrane 109 (in FIGURES 1A and 1B) and hemofilter membrane 209 (in FIGURE 2) are preferably organized as a parallel plate membrane or as a membrane hollow fiber. Preferred embodiments use a hemofilter incorporating the techniques and materials discussed in United States Patent Number 5,571,418, which is herein incorporated by reference, which discusses the use of large pore hemofiltration membranes for hemofiltration processes. Hemofilter membrane 109 in FIGURES 1A and 1B and hemofilter membrane 209 in FIGURE 2 are preferably comprised of large pore hemofiltration membranes, which are preferably fabricated from any biocompatible material suitable for the purpose such as polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-alcohol, polyamide, polycarbonate, cellulose derivatives, etc., but, of course, without limitation to these materials.

As shown in step 304 in FIGURES 3A and 3B, hemofilter membrane 109 (in FIGURES 1A and 1B) sieves a fraction of plasma water, electrolytes, blood peptides and proteins with a molecular size smaller than the pore size of the membrane to form ultrafiltrate stream 111 (in FIGURES 1A

and 1B), which is directed to adsorptive device 108 (in FIGURES 1A and 1B), which has one or more chambers containing adsorbent material of one or more types, via fifth tubing 112 (in FIGURES 1A and 1B). As shown in step 5 307 in FIGURES 3A and 3B, adsorptive device 108 is perfused by ultrafiltrate stream 111. Similarly, as shown in step 404 in FIGURE 4, hemofilter membrane 209 (in FIGURE 2) sieves a fraction of plasma water, electrolytes, blood peptides and proteins with a molecular size smaller than 10 the pore size of the membrane to form ultrafiltrate stream 211 (in FIGURE 2), which is directed to adsorptive device 208 (in FIGURE 2), which has one or more chambers containing adsorbent material of one or more types, via fifth tubing 212, and sixth tubing 215 (in FIGURE 2). As 15 shown in step 407 in FIGURE 4, adsorptive device 208 is perfused by ultrafiltrate stream 211.

As shown in steps 308 in FIGURES 3A and 3B, ultrafiltrate stream 115 (in FIGURES 1A and 1B) is divided at three-way stop cock or first three-way joint 110 (in 20 FIGURES 1A and 1B), after adsorptive device 108 in FIGURES 1A and 1B. As shown by step 408 in FIGURE 4, ultrafiltrate stream 211 (in FIGURE 2) is divided at three-way stop cock or first three-way joint 210 (in FIGURE 2), before adsorptive device 208 in FIGURE 2.

25 Specifically, in FIGURE 1A, after three-way stop cock or first three-way joint 110 divides post-adsorptive ultrafiltrate stream 115, discard ultrafiltrate stream 127 is directed toward second ultra-filtrate pump 106b and to waste reservoir 119 and return ultrafiltrate stream 131 is 30 directed toward first ultra-filtrate pump 106a and on to mammal 100. In FIGURE 1B, ultrafiltrate stream 115 is directed toward single ultrafiltrate pump 106 and discard ultrafiltrate stream 121 is directed to waste reservoir 119 and return ultrafiltrate stream 129 is returned to mammal 35 100. In FIGURE 2, ultrafiltrate stream 211 is directed

toward three stop cock 210 and discard ultrafiltrate stream 221 is directed toward second ultrafiltrate pump 206b and then onto waste reservoir 219 and return ultrafiltrate stream 229 is directed toward first ultrafiltrate pump 206a and eventually returned to mammal 200.

Adsorptive device 108 (in FIGURES 1A and 1B) and adsorptive device 208 (in FIGURE 2) have one or more chambers containing adsorbent material(s). The adsorbent material(s) is (are) preferably fixed or contained within the respective adsorbent device and none will pass into the ultrafiltrate stream or return to mammal 100 (in FIGURES 1A and 1B) and mammal 200 (in FIGURE 2). The adsorbent materials used in the preferred embodiment may be coated or uncoated. The nature of the adsorbent materials used in the preferred embodiment is such that solutes to be adsorbed will be bound to the adsorbent materials. As shown in FIGURE 5A, 5B, and 5C, adsorbent material is presented to ultrafiltrate flow by structures such as rods or plates, or flows through structures such as beads or porous matrix of any configuration effective in presentation of adsorptive material(s) to ultrafiltrate stream, or flows through one or more chambers containing immobilized particulate, beaded or fragmented adsorbent material. Adsorbent materials may include, but are not limited to: silica, activated charcoal, nonionic resins, ionic resins, immobilized polymyxin B, anion exchange resin, cation exchange resin, neutral exchange resin, immobilized monoclonal antibodies, immobilized IM receptors, immobilized specific antagonists, cellulose and its derivatives, synthetic materials (e.g., polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-alcohol, polyamide, polycarbonate, etc.) and the like or any combination thereof. The selection of adsorbent materials depends on the inflammatory mediators to be removed. Preferred embodiment uses polymyxin to remove

endotoxin, anti-TNF antibody to remove TNF, polyacrylonitrile to remove interleukin 1-beta and TNF, among other adsorbents, both specific and nonspecific. Adsorbents may also be used in various combinations as the patients condition and stage of disease warrant.

FIGURES 5A, 5B, and 5C are diagrams showing preferred embodiments of adsorptive device 108 (in FIGURE 1A and 1B) and adsorptive device 208 (in FIGURE 2), both of which have one or more chambers containing adsorbent material of one or more types. Adsorbent materials vary widely in their adsorptive capacity, and types and conditions of substances adsorbed. IM are of many different chemical types (e.g. peptides, lipids) and each IM's charge and plasma binding (e.g., specific or nonspecific circulating soluble receptors) will vary the characteristics of how they may be adsorbed during the course of any inflammatory mediator related disease ("IMRD") or episode of SIRS/MODS/MOSF. For this reason, various adsorbent materials will be used in order to provide the range of chemical binding characteristics and capacity needed for removal of many IM from ultrafiltrate. As stated above, adsorbent materials are of different chemical and physical types. Particulate adsorbent materials (e.g. charcoal; beads of polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-alcohol, polyamide, polycarbonate, cellulose derivatives, and similar materials; liposomes, etc.) may be coated or uncoated, but are usually encased in a porous flexible mesh sac or rigid porous containment jacket which allows free access of perfusing fluid (e.g. ultrafiltrate) but contains the particles and prevents them from being carried back to the mammal in the ultrafiltrate stream. Some adsorbents (e.g. silica gel) lend themselves to being cast or otherwise fabricated in various rigid or semirigid configurations (e.g. rods, plates etc.) which allow for effective and convenient presentation of ultrafiltrate

containing IM to the adsorbent material. Some adsorbents (e.g. monoclonal antibodies, IM receptors, specific antagonists, polymyxin B) will need to be affixed to a supporting matrix of biocompatible material (e.g. polycarbonate and the like) for presentation of adsorbent material to the ultrafiltrate stream containing IM. The matrix of biocompatible material will be configured to allow effective and convenient presentation of ultrafiltrate containing IM to the affixed adsorbent material.

Depending on physical and chemical compatibilities of the adsorbent materials, and the requirements of adequate ultrafiltrate flow, adsorbent device 108 (in FIGURES 1A and 1B) and adsorbent device 208 (in FIGURE 2) may be configured as one chamber containing one or more adsorbent materials, as shown in adsorptive device 508 in FIGURE 5A and adsorptive device 510 in FIGURE 5B, or separated into multiple chambers each containing one or more adsorbent materials, as shown in adsorptive device 512 in FIGURE 5C. Adsorbent devices 508 (in FIGURE 5A), 510 (in FIGURE 5B), and 512 (in FIGURE 5C) have an inlet port to which the ultrafiltrate tubing which carries the ultrafiltrate from hemofilter 108 (in FIGURES 1A and 1B) and hemofilter 208 (in FIGURE 2) will be attached to provide ultrafiltrate flow to adsorbent devices 508, 510, or 512. Ultrafiltrate flow through adsorbent device 508 (in FIGURE 5A), 510 (in FIGURE 5B), and 512 (in FIGURE 5C), perfuses the adsorbent materials allowing for adsorption of IM, and flows out of the adsorbent device through an outlet port.

Referring to FIGURE 5C, where a multiple chamber configuration is used for adsorptive device 512, the chambers will be separated by a screen or other porous barrier which retains the adsorbent materials or combinations of adsorbent materials in their separate compartments and allows free flow of ultrafiltrate through

adsorptive device 512. An alternative embodiment utilizes separate, exchangeable modules each containing an adsorbent material or adsorbent materials. A module or a combination of modules may be inserted into the adsorbent device to provide for the adsorption of different types of IM as the condition of the mammal may require. Although not shown, adsorbent device 108 (in FIGURES 1A and 1B) and adsorptive device 208 (in FIGURE 2) can be incorporated into or combine with hemofilter 102 (in FIGURES 1A and 1B) and hemofilter 202 (in FIGURE 2), respectively. In this embodiment ultrafiltrate formed at the hemofilter membrane will pass into the hemofilter jacket, the hemofilter jacket will incorporate the adsorptive materials in one or more chambers and ultrafiltrate will flow through the adsorbent materials. Ultrafiltrate will transfer from the combined hemofilter/adsorbent device through an outlet port to post adsorbent ultrafiltrate tubing.

The amount of blood continuously pumped will be operator determined and depend on the condition of mammal 100 (in FIGURES 1A and 1B) and mammal 200 (in FIGURE 2) and the needs of effective HF. The amount of blood continuously removed must be determined on a case by case basis. The flow rate, the amount of blood removed and the duration of the HF therapy are determined by the weight, the age and the nature and severity of illness of mammal. Typically, blood flow rates range from 100 to 200 ml/minute. The rate of ultrafiltration depends on the nature and severity of illness and is indexed to body weight, total body water and/or clinical indices of disease management (e.g., pulmonary function, cardiovascular status, etc.). Typically, total ultrafiltrate flow rate is 1 to 9 liters/hour of which from 0 to 2 liters/hour may be discarded. The discard rate will be determined by the fluid balance requirements of the mammal. The amount of ultrafiltrate discarded will be determined by operator as

operator judges the needs of mammal 100 and mammal 200 for fluid removal. All ultrafiltrate not discarded is returned to mammal 100 (in FIGURES 1A and 1B) and mammal 200 (in FIGURE 2).

5 With respect to the tubing used in preferred embodiments for tubing, the composition of the material making up the blood pump tubing, ultrafiltrate tubing, etc, is preferably of a biocompatible material, such as polyvinylchloride, but not limited to this material. The
10 tubing will be flexible and have outside diameters complementary to the appropriate hemofilter connections, adsorptive device connections, joints, stop cocks, or pump heads.

 Specifically, with respect to the tubing in FIGURE 1A,
15 first tubing 101 transfers blood from mammal 100 to blood pump 104; second tubing 103 transfers blood from blood pump 104 to hemofilter 102; third tubing 105 transfers the filtered blood filtered by hemofilter 102 to second three-way joint 125; fourth tubing 107 transfers the filtered
20 blood along with the post adsorption ultrafiltrate to mammal 100; fifth tubing 112 transfers the ultrafiltrate to adsorptive device 108; sixth tubing 123 transfers the post adsorption ultrafiltrate to three-way stop cock or second three-way joint 110; seventh tubing 131 transfers post
25 adsorption ultrafiltrate to first ultrafiltrate pump 106a; eighth tubing 129 transfers post adsorption ultrafiltrate from first ultrafiltrate pump 106a to second three-way joint 125 joining fourth tubing 107 which transfers filtered blood along with the post adsorption
30 ultrafiltrate to the mammal; ninth tubing 127 transfers post adsorption ultrafiltrate to second ultrafiltrate pump 106b; and tenth tubing 121 transfers post adsorption ultrafiltrate from second ultra filtrate pump 106b to waste reservoir 119. First ultrafiltrate pump 106a and
35 associated tubing implement steps 311 and 312 in FIGURE 3A;

second ultrafiltrate pump 106b, waste reservoir 119, and associated tubing implement steps 309 and 310 in FIGURE 3A.

With respect to the tubing in FIGURE 1B, first tubing
5 101 transfers blood from mammal 100 to blood pump 104;
second tubing 103 transfers blood from blood pump 104 to
hemofilter 102; third tubing 105 transfers the filtered
blood filtered by hemofilter 102 to second three-way joint
125; fourth tubing 107 transfers the filtered blood along
10 with the post adsorption ultrafiltrate to mammal 100; fifth
tubing 112 transfers the ultrafiltrate to adsorptive device
108; sixth tubing 123 transfers the post adsorption
ultrafiltrate or ultrafiltrate stream 115 to single
ultrafiltrate pump 106; seventh tubing 127 transfers post
15 adsorption ultrafiltrate from ultrafiltrate pump 106 to
three-way stop cock or first three-way joint 110; eighth
tubing 129 transfers post adsorption ultrafiltrate from
three-way stop cock or first three-way joint 110 to second
three-way joint 125 joining fourth tubing 107 which
20 transfers filtered blood along with the post adsorption
ultrafiltrate to mammal 100; and ninth tubing 121 transfers
post adsorption ultrafiltrate from three-way stop cock or
first three-way joint 110 to waste reservoir 119. Single
ultrafiltrate pump 106 and associated tubing implement step
25 351 in FIGURE 3B; waste reservoir 119 and associated tubing
implement step 310 in FIGURE 3B. Second three-way joint
125 and associated tubing implement step 312 in FIGURE 3B.

With respect to the tubing in FIGURE 2, first tubing
30 201 transfers blood from mammal 200 to blood pump 204;
second tubing 203 transfers blood from blood pump 204 to
hemofilter 202; third tubing 205 transfers the filtered
blood filtered by hemofilter 202 to second three-way joint
225; fourth tubing 207 transfers the filtered blood along
35 with the post adsorption ultrafiltrate to mammal 200; fifth

tubing 212 transfers the ultrafiltrate to three-way stop
cock or first three-way joint 210; sixth tubing 215
transfers the ultrafiltrate from three-way stop cock or
first three-way joint 210 to adsorptive device 208; seventh
5 tubing 229 transfers the post adsorption ultrafiltrate or
ultrafiltrate stream 215 to first ultrafiltrate pump 206a;
eighth tubing 223 transfers post adsorption ultrafiltrate
from first ultrafiltrate pump 206a to second three-way
joint 225 joining fourth tubing 207 which transfers
10 filtered blood along with the post adsorption
ultrafiltrate to mammal 200; ninth tubing 225 transfers
ultrafiltrate from three-way stop cock or first three-way
joint 210 to second ultrafiltrate pump 206b; and tenth
tubing 233 transfers ultrafiltrate from second
15 ultrafiltrate pump 206b to waste reservoir 219. First
ultrafiltrate pump 206a and associated tubing implement
steps 411 and 412 in FIGURE 4; second ultrafiltrate pump
206b and waste reservoir 219 and associated tubing
implement steps 409 and 410 in FIGURE 4.

20

Further Modifications and Variations

Although the invention has been described with
reference to a specific embodiment, this description is not
meant to be construed in a limiting sense. The example
25 embodiments shown and described above are only intended as
an example. Other applications of the preferred
embodiments may be found as well. Various modifications of
the disclosed embodiment as well as alternate embodiments
of the invention will become apparent to persons skilled in
30 the art upon reference to the description of the invention.

For instance, structural modification could include the
integration of hemofilter 102 in FIGURES 1A and 1B and
hemofilter 202 in FIGURE 2 with adsorptive device 108 (in
FIGURES 1A and 1B) and adsorptive device 208 (in FIGURE 2),
35 both of which have one or more chambers containing

adsorbent material of one or more types, with elimination of the additional tubing. In this embodiment ultrafiltrate formed in jacket of hemofilter 102 (in FIGURES 1A and 1B) and hemofilter 202 (in FIGURE 2) would be presented directly to adsorbent material contained within hemofilter jacket or in a chamber or chambers directly contiguous with hemofilter jacket. The chamber containing ultrafiltrate would be drained by ultrafiltrate line. Ultrafiltrate would be continuously pumped and apportioned for discard or returned to mammal 100 (in FIGURES 1A and 1B) and mammal 200 (in FIGURE 2). In addition, it is possible to modify the configuration of ultrafiltrate lines to provide for infusion of ultrafiltrate into mammal 100 (in FIGURES 1A and 1B) or mammal 200 (in FIGURE 2) via a vascular cannula in a blood vessel and separate from the hemofiltration circuit. Furthermore, note the ultrafiltrate return pump and the ultrafiltrate discard pump in the preferred embodiment shown and discussed above may be combined into a single two head ultrafiltrate pump system. Also, note while the ultrafiltrate return pump and the ultrafiltrate discard pump are shown in the figures as two separate pumps, it is within the scope of the invention to combine two pumps into a single pump, and thus, the separate pumps may be interpreted as two parts of a single pump.

Modifications of adsorbent device will be determined by the inflammatory mediator related disease (IMRD) to be treated and the phase of the disease. Various regions of the IM network are dominant at different phases of an IMRD and different IMRD exhibit different patterns of IM networking. Thus a different adsorbent material or materials, or different groupings of adsorbent materials will be needed for different IMRD's in their different phases. Thus different adsorbent devices will be developed as more is learned of IMRD's and their phases. Adsorbent devices may contain a fixed adsorbent material or a fixed

combination of adsorbent materials. Alternatively, an adsorbent device may be configured with different, interchangeable modules of adsorbent materials to be adapted to the changing dominance of the IM network. The modules may consist of one or more chambers containing adsorbent material of one or more types. The adsorbent device may be designed to accept modules of adsorbent materials inserted in place as dictated by patient need and operator assessment.

Different configurations of adsorbent materials will be used. Adsorbent materials exhibit chemical characteristics which determine what physical form will provide the greatest stability in flowing ultrafiltrate. Adsorbent material must remain irreversibly bound to its supporting matrix, or in the case of beads (e.g. polysulfone, polyacrylonitrile, etc) or particulates (e.g. charcoal) inescapably contained in mesh or other containment device. Adsorbent material, matrix, and containment material can not be allowed to dissolve, dissociate or fragment into the ultrafiltrate to be infused into the mammal. Adsorbent material, matrix, and containment material must be configured to provide physical durability, and adequate porosity and configuration for optimal presentation of adsorbent material to flowing ultrafiltrate. Some configurations of matrix are shown in FIGURES 5A, 5B, and 5C. Adsorbent devices of one or more chambers containing adsorbent material of one or more types could be used in series, in which ultrafiltrate flows from the first to subsequent adsorbent devices. The sequence, number and type of adsorbent devices would be determined by operator to meet the needs of mammal. Alternatively, the ultrafiltrate stream could be divided by a manifold with distribution of ultrafiltrate to adsorbent devices arranged in a parallel configuration, with each line from each adsorbent device either returned to a

manifold and reunited into a single ultrafiltrate line, or each line individually apportioned for return to mammal and discard.

5 Thus, even though numerous characteristics and advantages of the present inventions have been set forth in the foregoing description, together with details of the structure and function of the inventions, the disclosure is illustrative only, and changes may be made in the detail, especially in matters of shape, size and arrangement of the parts within the principles of the inventions to the full extent indicated by the broad general meaning of the terms used in the attached claims. Accordingly, it should be understood that the modifications and variations suggested above and below are not intended to be exhaustive. These 10 examples help show the scope of the inventive concepts, which are covered in the appended claims. The appended claims are intended to cover these modifications and alternate embodiments. 15

In short, the description and drawings of the specific examples above are not intended to point out what an infringement of this patent would be, but are to provide at least one explanation of how to make and use the inventions contained herein. The limits of the inventions and the bounds of the patent protection are measured by and defined 20 in the following claims. 25

WHAT IS CLAIMED IS:

1. A hemofiltration system to treat inflammatory mediator related disease in a mammal, comprising:

5 (a) a hemofilter to receive blood removed from said mammal, said hemofilter removes ultrafiltrate from said blood from said mammal to create filtered blood, said filtered blood is returned to said mammal; and

10 (b) an adsorptive device containing adsorbent material to receive ultrafiltrate removed from said blood from said mammal, said adsorbent material or adsorbent materials removes inflammatory mediators that cause said inflammatory mediator related disease from said ultrafiltrate removed from said blood of said mammal to create post adsorption ultrafiltrate, said post adsorption
15 ultrafiltrate is combined with said filtered blood and returned to said mammal.

2. The hemofiltration system of Claim 1, wherein said adsorbent material is selected from a group consisting
20 of activated charcoal, uncharged resins, charged resins, silica, immobilized polymyxin B, anion exchange resin, cation exchange resin, neutral exchange resin, polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-alcohol, polyamide, polycarbonate, cellulose derivatives,
25 immobilized monoclonal antibodies, immobilized IM receptors, immobilized specific antagonists, and any combination thereof.

3. The hemofiltration system of Claim 1, wherein
30 said adsorbent material is comprised of a material selected from a group consisting of coated materials, uncoated materials, a matrix of rods, a matrix configured for convenient and effective presentation of ultrafiltrate to adsorbent materials, beads, and particulates and any
35 combination thereof.

4. The hemofiltration system of Claim 1, wherein said adsorbent material prevents dissolution and fragmentation of adsorbent material, or where said adsorptive device contains said fragments.

5

5. The hemofiltration system of Claim 1, wherein said adsorbent material is comprised of adsorbent resins selected from a group consisting of polymyxin B immobilized, polystyrene-derivative fibers, anion exchange resins, cation exchange resins, neutral exchange resins, cellulose materials, polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-alcohol, polyamide, polycarbonate, cellulose derivatives, specific antagonist coated materials and specific antibody coated materials.

10

15

6. The hemofiltration system of Claim 1, wherein said hemofilter sieves said ultrafiltrate, said ultrafiltrate comprised of plasma water, electrolytes, blood peptides, proteins, carbohydrates, and lipids.

20

7. The hemofiltration system of Claim 6, wherein said hemofilter has a membrane having at least one pore, said at least one pore having a pore size, said blood peptides and proteins have a molecular size smaller than said pore size of said at least one pore of said membrane.

25

8. The hemofiltration system of Claim 1, further comprising:

- © a blood pump to pump said blood from said mammal;
- (d) an ultrafiltrate return pump to pump said post
5 adsorbent ultrafiltrate;
- (e) an ultrafiltrate waste pump to pump said post
adsorbent ultrafiltrate;
- (f) a three-way stop cock;
- (g) a three-way joint;
- 10 (h) first tubing to transfer said blood from said
mammal to said blood pump;
- (I) second tubing to transfer said blood from said
blood pump to said hemofilter;
- (j) third tubing to transfer said filtered blood
15 filtered by said hemofilter to said three-way joint;
- (k) fourth tubing to transfer said filtered blood
along with said post adsorptive ultrafiltrate to said
mammal;
- (l) fifth tubing to transfer said ultrafiltrate from
20 said hemofilter to said adsorptive device;
- (m) sixth tubing to transfer said post adsorptive
ultrafiltrate to said three-way stop cock;
- (n) seventh tubing to transfer said post adsorptive
ultrafiltrate to said ultrafiltrate return pump;
- 25 (o) eighth tubing to transfer said post adsorptive
ultrafiltrate to said three-way joint;
- (p) ninth tubing to transfer said post adsorptive
ultrafiltrate from said three-way stop cock to said
ultrafiltrate waste pump; and
- 30 (q) tenth tubing to transfer said post adsorptive
ultrafiltrate from said ultrafiltrate waste pump to said
waste reservoir.

9. The hemofiltration system of Claim 1, wherein
35 said hemofilter is comprised of a biocompatible material.

10. The hemofiltration system of Claim 1, wherein
said hemofilter is comprised of a membrane and a jacket,
wherein said membrane is selected from the group of
polysulfone, polyacrylonitrile, polymethylmethacrylate,
5 polyvinyl-alcohol, polyamide, polycarbonate, cellulose
derivatives and said jacket is comprised of polycarbonate.

11. A hemofiltration system to treat inflammatory mediator related disease in a mammal, comprising:

(a) a hemofilter to remove ultrafiltrate from a blood stream extracted from said mammal to create a filtered blood stream and an ultrafiltrate stream; and

(b) an adsorptive device of adsorbent material to receive said ultrafiltrate stream received from said hemofilter to remove inflammatory mediators to create a post adsorption ultrafiltrate stream, said post adsorption ultrafiltrate stream selectively combined with said filtered blood stream and returned to said mammal.

12. The hemofiltration system of Claim 11, wherein said adsorbent material is selected from a group consisting of activated charcoal, uncharged resins, charged resins, silica, immobilized polymyxin B, anion exchange resin, cation exchange resin, neutral exchange resin, polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-alcohol, polyamide, polycarbonate, cellulose derivatives, immobilized monoclonal antibodies, immobilized IM receptors, immobilized specific antagonists, and any combination thereof.

13. The hemofiltration system of Claim 11, wherein said adsorbent material is comprised of a material selected from a group consisting of coated materials, uncoated materials, a matrix of rods, a matrix configured for convenient presentation of ultrafiltrate to adsorbent material, beads, and particulates and any combination thereof.

14. The hemofiltration system of Claim 11, wherein said adsorbent material prevents dissolution and fragmentation of adsorbent material or where said adsorptive device contains said fragments.

15. The hemofiltration system of Claim 11, wherein said adsorbent material is comprised of adsorbent resins selected from a group consisting of immobilized polymyxin B , polystyrene-derivative fibers, cation exchange resins, neutral exchange resins, anion exchange resins, cellulose materials, polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-alcohol, polyamide, polycarbonate, cellulose derivatives, specific antibody coated materials, specific antagonist coated materials, and any combination thereof.

16. The hemofiltration system of Claim 11, wherein said hemofilter sieves said ultrafiltrate stream, said ultrafiltrate stream comprised of plasma water, electrolytes, and blood peptides and proteins.

17. The hemofiltration system of Claim 16, wherein said hemofilter has a membrane having at least one pore, said at least one pore having a pore size, said blood peptides and proteins have a molecular size smaller than said pore size of said at least one pore of said membrane.

18. The hemofiltration system of Claim 11, further comprising:

© a blood pump to pump said blood stream from said mammal;

5 (d) an ultrafiltrate waste pump to pump said post adsorption ultrafiltrate stream to said waste reservoir and an ultrafiltrate return pump to pump said post adsorption ultrafiltrate stream to combine with said filtered blood stream;

10 (e) a three-way stop cock to direct said ultrafiltrate stream;

(f) a three-way joint to combine said filtered blood stream with said post adsorption ultrafiltrate stream;

15 (g) first tubing to transfer said blood stream from said mammal to said blood pump;

(h) second tubing to transfer said blood stream from said blood pump to said hemofilter;

20 (I) third tubing to transfer said filtered blood stream filtered by said hemofilter to said three-way joint;

(j) fourth tubing to transfer said filtered blood stream along with said post adsorption ultrafiltrate stream to said mammal;

25 (k) fifth tubing to transfer said ultrafiltrate stream to said three-way stop cock;

(l) sixth tubing to transfer said ultrafiltrate stream from said three-way stop cock to said adsorptive device;

30 (m) seventh tubing to transfer said post adsorption ultrafiltrate stream to said ultrafiltrate return pump;

(n) eighth tubing to transfer said post adsorption ultrafiltrate stream from said ultrafiltrate return pump to said three-way joint of said fourth tubing;

(o) ninth tubing to transfer said ultrafiltrate stream from said three-way stop cock to said ultrafiltrate waste pump; and

5 (p) tenth tubing to transfer said ultrafiltrate from said ultrafiltrate waste pump to said waste reservoir.

19. The hemofiltration system of Claim 11, wherein said hemofilter is comprised of a biocompatible material.

10 20. The hemofiltration system of Claim 11, wherein said hemofilter is comprised of a membrane and a jacket, wherein said membrane is selected from the group of polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-alcohol, polyamide, polycarbonate, and cellulose
15 derivatives, and said jacket is comprised of polycarbonate.

21. A hemofiltration process used to treat inflammatory mediator related disease in a mammal, comprised of the following steps:

5 (a) removing blood from said mammal to create a blood stream;

(b) filtering said blood stream to remove ultrafiltrate from said blood to create an ultrafiltrate stream and a filtered blood stream;

10 © circulating said ultrafiltrate stream to an adsorptive device to remove inflammatory mediators that cause said inflammatory mediator related disease to create a post adsorbent ultrafiltrate stream;

15 (d) combining said post adsorbent ultrafiltrate stream with said filtered blood stream to create a post adsorbent ultrafiltrate/filtered blood stream; and

(e) returning said post adsorbent ultrafiltrate/filtered blood stream to said mammal.

20 22. The process of Claim 21, wherein an adsorptive device contains adsorbent material, said adsorbent material adsorbs inflammatory mediators from said ultrafiltrate stream.

25 23. The process of Claim 22, wherein said adsorbent material is selected from a group consisting of activated charcoal, uncharged resins, charged resins, silica, immobilized polymyxin B, anion exchange resin, cation exchange resin, neutral exchange resin, polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-
30 alcohol, polyamide, polycarbonate, cellulose derivatives, immobilized monoclonal antibodies, immobilized IM receptors, immobilized specific antagonists, and any combination thereof.

24. The process of Claim 22, wherein said adsorbent material is comprised of a material selected from a group consisting of coated materials, uncoated materials, a matrix of rods, a matrix configured for effective presentation of adsorbent material to said ultrafiltrate stream, and beads.

25. The process of Claim 22, wherein said adsorbent material prevents dissolution and fragmentation of adsorbent material into said ultrafiltrate stream, or where said adsorptive device contains said fragments.

26. The process of Claim 22, wherein said adsorbent material is comprised of resins selected from a group consisting of immobilized polymyxin B, polystyrene-derivative fibers, charged exchange resins, neutral exchange resins; polysulfone, polyacrylonitrile, polymethylmethacrylate, polyvinyl-alcohol, polyamide, polycarbonate, etc.) and cellulose derivatives, specific antagonist coated materials, and specific antibody coated materials.

27. The process of Claim 21, wherein a hemofilter is used to remove said ultrafiltrate from said blood stream to create said filtered blood stream and said ultrafiltrate stream, said hemofilter sieves said ultrafiltrate stream, said ultrafiltrate comprised of plasma water, electrolytes, and blood peptides and proteins.

28. The hemofiltration system of Claim 27, wherein said hemofilter has a membrane having at least one pore, said at least one pore having a pore size, said blood peptides and proteins have a molecular size smaller than said pore size of said at least one pore of said membrane.

29. The hemofiltration system of Claim 11, further comprising

after step (a),

(a1) pumping said blood stream;

5 and after step (c),

(c1) pumping said post adsorption ultrafiltrate stream.

30. The process of Claim 27, wherein said hemofilter
10 is comprised of a biocompatible material.

31. The hemofiltration system of Claim 27, wherein
said hemofilter is comprised of a membrane and a jacket,
wherein said membrane is selected from the group of
15 polysulfone, polyacrylonitrile, polymethylmethacrylate,
polyvinyl-alcohol, polyamide, polycarbonate, and cellulose
derivatives, and said jacket is comprised of
polycarbonate.

FIG. 1B

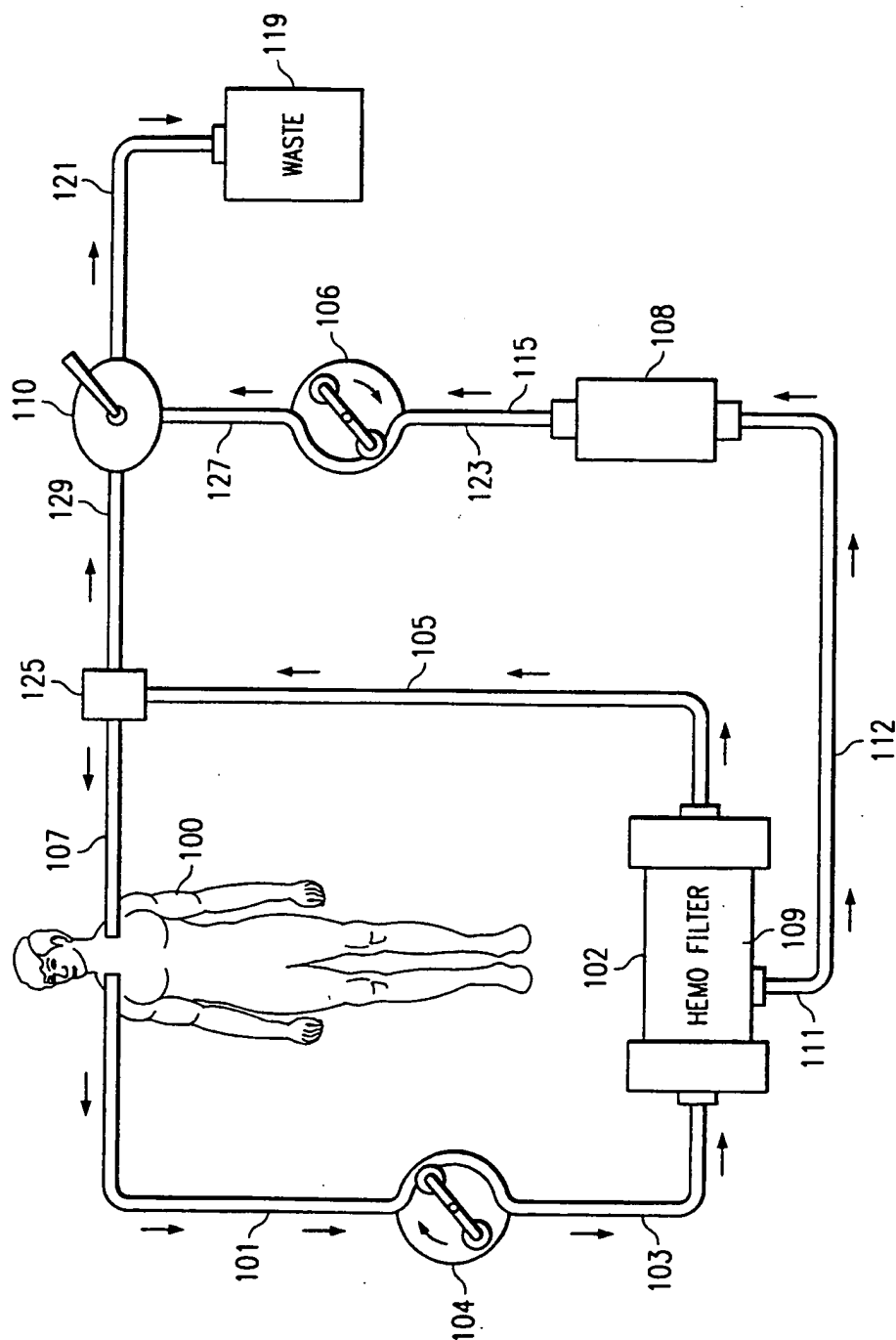


FIG. 2

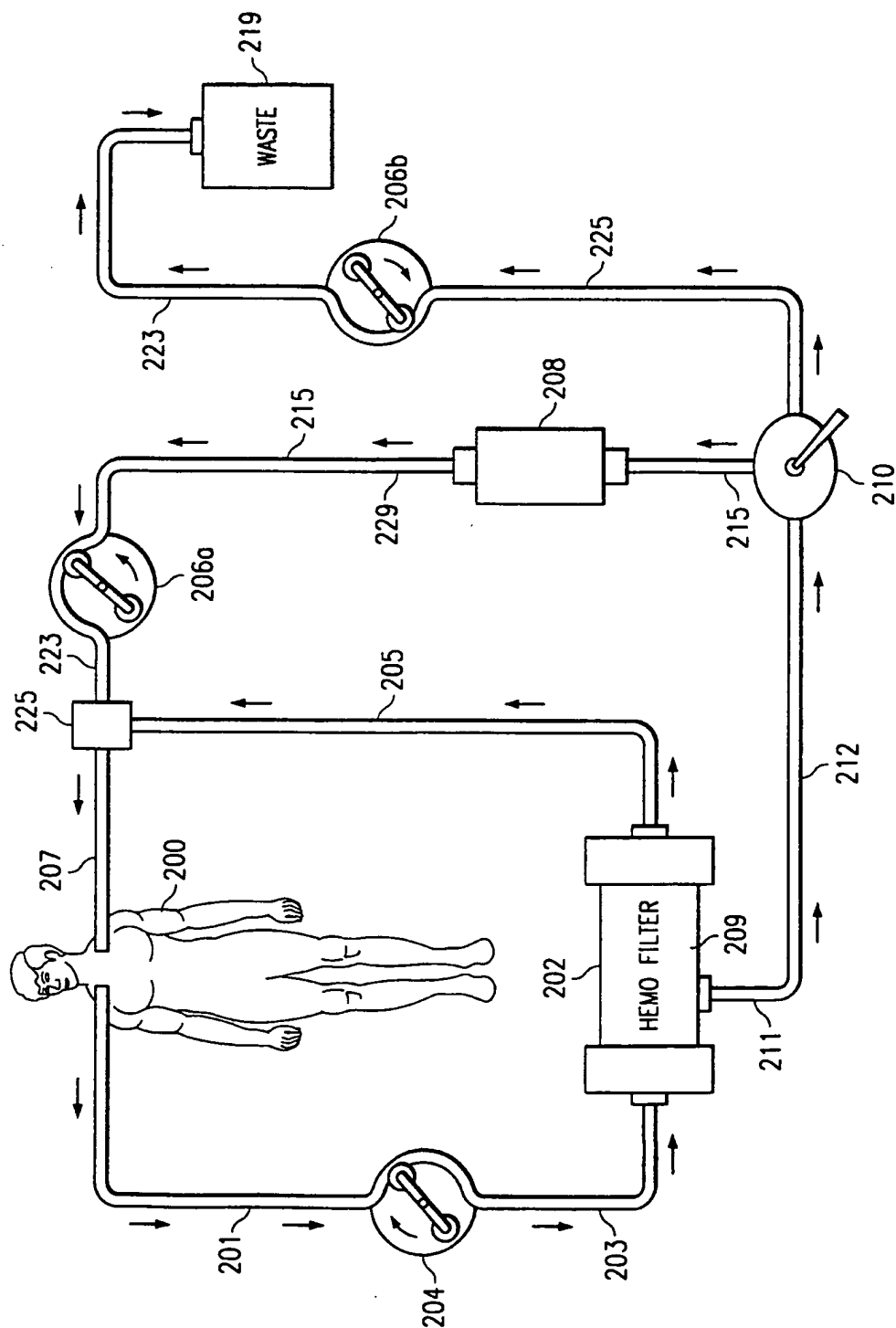
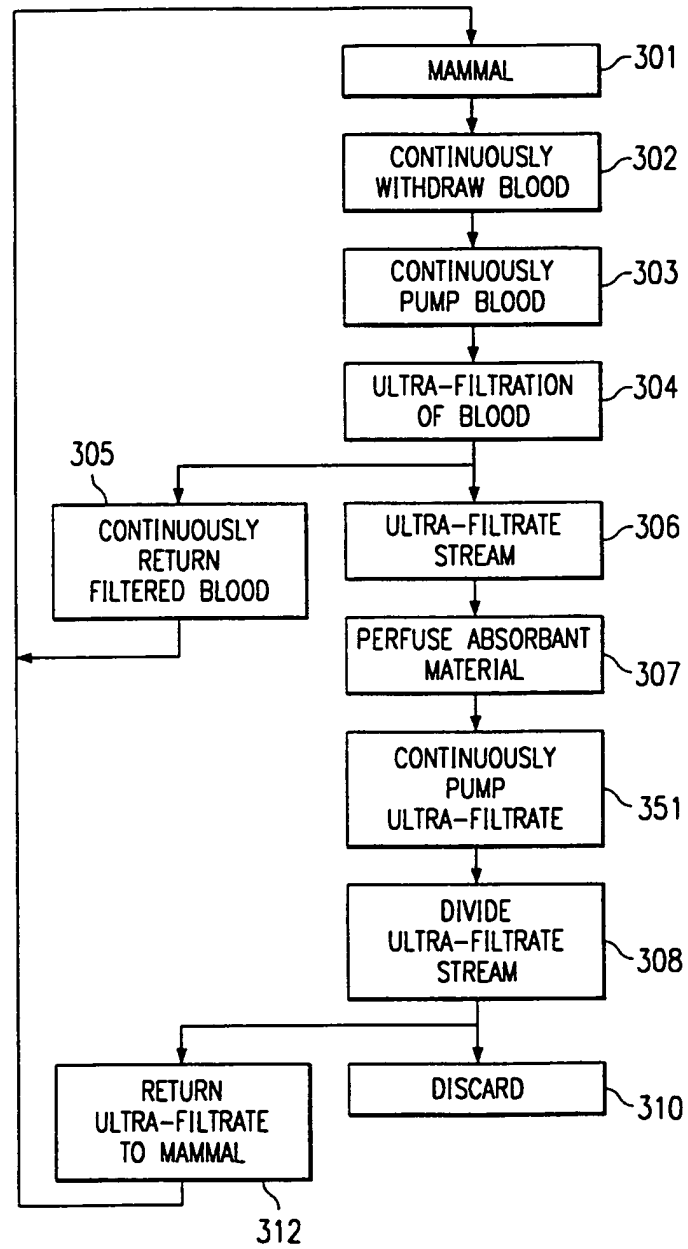


FIG. 3



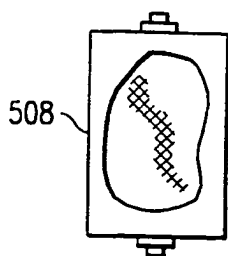
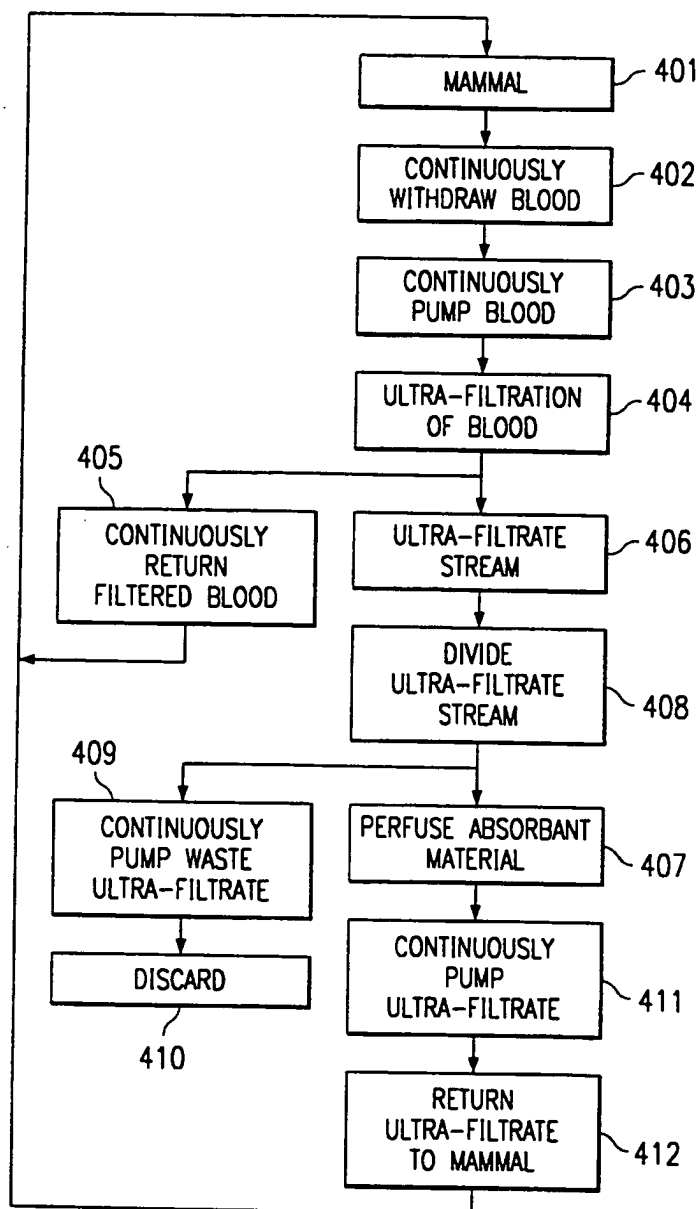


FIG. 5A

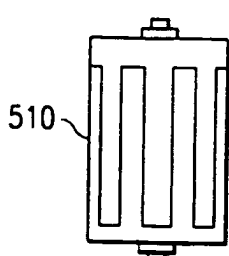


FIG. 5B

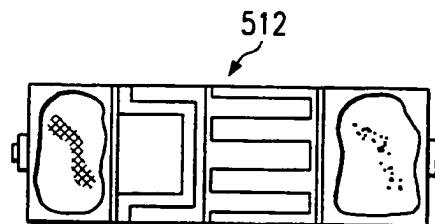


FIG. 5C